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Patent Application

of:

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for

Method of Removing High Density Stickies from Secondary Papermaking Fibers

METHOD OF REMOVING HIGH DENSITY STICKIES FROM SECONDARY
PAPERMAKING FIBERS

5 Cross-Reference to Related Applications and Claim for Priority

 This application is a continuation-in-part application of co-pending
Application Serial No. 09/772,395, filed January 30, 2001, now United States Patent
No. _____, which in turn was based upon Provisional Application Serial
No. 60/180,348, filed February 4, 2000. The priority of the foregoing applications,
10 both entitled "Hybrid Multistage Forward Cleaner System With Flotation Cell", is
hereby claimed.

Technical Field

 The present invention relates generally to papermaking fiber processing and
15 more particularly to a method useful for removing stickies from secondary or recycle
paper pulp by incorporating a hybrid multistage forward cleaner system with an
integrated flotation cell. The method is particularly effective for removing stickies
that have already passed through a screening stage.

20 Background

 Processing of papermaking fibers to remove contaminants is well known in
the art, including the use of forward cleaners and flotation cells. Such technology is
used, for example, to treat secondary (recycle) fiber sources for re-use in paper
products such as towel and tissue, paperboard, coated writing and printing papers and
25 so forth. Equipment utilized includes screening devices, flotation cells and the like as
may be seen, for example, in United States Patent Nos. 4,272,315 to *Espenmiller*;
4,983,258 to *Maxham*; 5,240,621 to *Elonen et al.*; and 5,693,222 to *Galvan et al.*

Recycling paper into secondary pulp suitable for re-use in high quality products is a relatively complex, capital intensive undertaking as will be appreciated from United States Patent No. 5,587,048 to *Streisel et al.* The basic cleaning sequence of the '048 patent is as follows: (1) detrashing - the detrasher contains 6mm (1/4 inch) holes and retains large contaminants, such as plastic bags, pieces of wood, large staples, pieces of metal and packing tape, detrashing typically takes place at 3-5% solids; (2) high-density cleaning - heavy, coarse contaminants, such as bolts, staples and rocks are removed, high density cleaning typically takes place at about 3-4% solids; (3) primary coarse screening - primary coarse screens contain holes 2-3 mm in size, preferably 2.4 mm, for removing medium-sized contaminants, such as small fragments of wood, tape and styrofoam, coarse screening at this stage protects fine slotted screens downstream from being overwhelmed by contaminants that are large relative to the slot width, and results in improvement in quality and production rates, coarse screening typically takes place at about 2.5-3.5% solids; (4) secondary coarse screening - the rejects from the primary coarse screening may be screened again using holes of the same size, but at a lower consistency, about 1.5-2.5% solids; (5) sand cleaning (centrifugal) - sand cleaning at this stage protects the fine slotted screens downstream from excess wear, waste corrugated paperboard contains relatively large amounts of sand, cleaning ahead of the screen increases the cost of the system, and increases the requirements for hydraulic capacity, sand cleaning typically takes place at about 1% solids; (6) screening - fine slotted screens are used with a width of 0.008 inch (0.20 mm), rather than 0.012 inch previously used for corrugated paperboard, the fine screens remove plastic slivers, wax and stickie agglomerates, screening takes place at less than 1% solids, preferably less than 0.9%; (7) Lightweight Cleaning (*Gyrocleaning*) - lightweight cleaning preferentially removes materials with a specific gravity below 1.0, such as plastics, waxes and stickies, not heretofore removed, lightweight cleaning is performed at about 0.8% solids.

It should be appreciated from the '048 patent that existing methods for handling stickies removal were based on removing light contaminants having a density generally less than the fiber being cleaned. Such methods have been found inadequate when a significant amount of heavy stickies are present.

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The disclosures of the foregoing patents are hereby incorporated by reference.

Summary of Invention

10 In the past there were mainly small light weight stickies that managed to get through screens, and most of these small light weight stickies were subsequently removed by the gyro-cleans. More recently, heavy weight stickies started becoming a problem; presumably because some of the new pressure sensitive adhesives tend to form heavy weight stickies. The small heavy weight stickies, which managed to get through screens, were also accepted by the gyro-cleans or reverse cleaners, but they
15 were subsequently rejected with alot of fiber by the forward cleaners. Since the heavy weight stickies from the forward cleaners are still hydrophobic, it is possible to selectively remove them with a flotation cell after the hydrophobic particles attach themselves to air bubbles in the flotation cell.

20 The heavy weight stickies are difficult to remove by flotation if they lose their hydrophobic properties during the deinking process (e.g., due to the addition of dispersing chemicals) or if the flotation cell is operated inefficiently (e.g., at too high a consistency or with insufficient air bubbles or due to inadequate contact between stickies and air bubbles).

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One advantage of having the flotation cell on the forward cleaner rejects is that it is possible to keep the consistency low, since only 10 - 30% of the total flow is being treated (the percentage depends on reject flow amount). If all the stock is treated in a flotation cell, the tendency is to raise the consistency from 0.5 - 0.6% to

1% or higher to keep the size and cost of the equipment down. If the design consistency is already 1%, the heavy weight stickies removal efficiency becomes even worse when the consistency rises above 1% due to production increases. By installing a flotation cell on the forward cleaner rejects in an existing process, it is possible to design the hybrid cleaner flotation cell system at 0.5 - 0.6% consistency and obtain improved heavy weight stickies removal efficiency.

The present invention generally includes a method of processing secondary fiber to remove high density stickies which have a density generally greater than the fiber including: (a) processing a fiber feed stream to generate a rejects stream enriched in high density stickies and (b) treating the rejects stream enriched in high density stickies with a flotation stage to generate an intermediate flotation purified stream with a reduced high density stickies content. Preferably, the feed stream is initially processed by way of a centrifugal separation technique, such as feeding the stream to a bank of hydrocyclones, which generate a rejects stream enriched in high density stickies. The high density stickies typically have a characteristic area (that is, projected maximum cross-sectional area) of less than about 0.5 mm^2 , and usually less than about 0.3 mm^2 . The treatment by the flotation stage is effective to remove at least about 40 percent of the high density stickies present and, in most cases, at least about 50 percent. The high density stickies are believed to be derived from pressure sensitive adhesives.

In another aspect of the invention there is provided a method of thin stock processing secondary fiber to remove high density stickies having a density generally greater than the fiber includes the steps of: (a) processing a feed thin stock stream at a consistency of less than about 2.5%, preferably less than about 1%, to generate a thin stock accepts stream and a thin stock rejects stream, the thin stock rejects stream being enriched in high density stickies; and (b) treating the thin stock rejects stream enriched in high density stickies to generate an intermediate flotation purified stream.

The present invention provides in still another aspect a hybrid system for processing papermaking fibers and includes a multistage array of forward cleaners coupled with a flotation cell which increases overall efficiency of the system. In a typical embodiment, a first rejects aqueous stream from a first stage bank of centrifugal cleaners is treated in a flotation cell before being fed to a second stage bank of centrifugal cleaners. The accepts stream of the first stage bank of centrifugal cleaners is fed forward as is the accepts stream of the second stage bank of centrifugal cleaners. Preferably, the two accepts streams are combined.

One advantage of feeding the second accepts stream forward is that it does not have to be returned to the first bank of cleaners for re-cleaning. This reduces the size of the first bank of cleaners or allows an existing installation to operate at a lower consistency. (The cleaners operate more efficiently at a low consistency of 0.5% than at 0.8 or 1%). Another advantage is that the flotation cell typically operates at greater than 60% efficiency on removing hydrophobic contaminants from the first cleaner rejects, while another cleaner stage removes less than 50% of the hydrophobic contaminants. As a result a large quantity of hydrophobic contaminants are removed in the flotation stage, which makes the remaining cleaner stages work more efficiently with less good fiber loss.

As will be appreciated by one of skill in the art, the size and cost of a flotation stage for treating secondary fiber can be reduced by up to 75% if it is installed in centrifugal cleaner system as compared to a full scale treatment of the stock by flotation. The centrifugal cleaner system modeling indicates a 34% reduction in ink speck area of total centrifugal cleaner system accepts by removing ink specks from the first stage rejects with 80% efficiency in a flotation stage and then feeding the flotation accepts forward after centrifugal cleaning of the second stage. (24% reduction if second stage rejects are treated in a similar manner). The ability to feed the centrifugal cleaner rejects forward (after the flotation stage and additional

centrifugal cleaning in the next stage) reduces the stock consistency in the first stage, thereby improving the efficiency of the first stage. The capacity of the system is also increased by feeding the second stage centrifugal cleaner accepts forward. The other centrifugal cleaner stages can also be operated more efficiently since more than 50% of the ink in the first stage centrifugal cleaner rejects has been removed in the flotation stage. When the centrifugal cleaner accepts are thickened in a press, a large amount of ink ends up in the pressate. This ink can also be removed by using the ink-laden pressate as dilution water for the centrifugal cleaner rejects going to the flotation stage.

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A conventional centrifugal cleaner system (as shown in Figure 1) normally consists of several stages, whereby the rejects of each centrifugal cleaner stage are diluted for cleaning in the next stage and the centrifugal cleaner accepts are fed backwards to the feed of the previous stage. The ink speck removal efficiency of the centrifugal cleaner is usually much less than 50% on toner inks in office waste paper. As a result the total centrifugal cleaner system ink speck removal efficiency can drop to 30% or less on a furnish containing a large proportion of office waste.

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By sending the first or second stage centrifugal cleaner rejects to a flotation stage (as shown in Figure 2) it is possible to remove a much higher percentage of the ink specks in office waste. (It was possible to obtain 80% removal of ink specks during a pilot plant trial with a flotation cell operated on second stage centrifugal cleaner rejects.) If the accepts of the flotation cell are cleaned in the next centrifugal cleaner stage, the centrifugal cleaner accepts from that stage can then be fed forward to the thickener. Sending centrifugal cleaner accepts forward reduces the load and improves the efficiency of the previous centrifugal cleaner stage.

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The present invention is particularly useful in connection with removing stickies from a thin stock recycle fiber product stream; likewise, it is believed pitch

removal is enhanced. Stickies are generally a diverse mixture of polymeric organic materials which can stick on wires, felts or other parts of paper machines, or show on the sheet as "dirt spots" or holes. The sources of stickies may be pressure-sensitive adhesives, hot melts, waxes, latexes, binders for coatings, wet strength resins, or any of a multitude of additives that might be contained in recycled paper. The term "pitch" normally refers to deposits composed of organic compounds which are derived from natural wood extractives, their salts, coating binders, sizing agents, and defoaming chemicals existing in the pulp. Although there are some discrete characteristics, there are common characteristics between stickies and pitch, such as hydrophobicity, low surface energy, deformability, tackiness, and the potential to cause problems with deposition, quality, and efficiency in the process. Indeed, it is possible with the present invention to reduce stickies by 50%, 80% or even more by employing a flotation cell in a multistage forward cleaner system as hereinafter described in detail. The rejects from the flotation stage are so full of ink, ash and stickies that they can be rejected without any further treatment.

As will be appreciated from the discussion which follows, a preferred method of cleaning recycle pulp includes combining the accepts from a first centrifugal stage with the accepts from a second centrifugal stage which is fed with the flotation-purified rejects of the first stage. The process is particularly effective for removing relatively heavy weight (small size) hydrophobic stickies that have already passed through a screening stage. This will increase productivity of a paper machine utilizing the pulp and decrease paper machine downtime and converting downtime. Stickies build up on wires or fabrics and cause holes to form in the sheet requiring downtime on the paper machine to remove them. Stickies also build up on doctor blades in paper machines and get into the dewatering felt and so forth. In converting, they can cause problems such as sheets sticking together. They clog emboss rolls and interfere with the proper operation of other rolls, cause holes in the sheet and so on.

Solvents are typically required to remove stickies from equipment and this can lead to environmental issues.

5 In recent years, stickies removal from recycle fiber has become more difficult in many cases. Without intending to be bound by any theory, it is believed that stickies generated from waste paper including pressure-sensitive adhesives become more flexible at typical operating temperatures (40°C) of screens and thus tend to pass through even fine screens.

10 The method of the present invention has been employed in a commercial papermill and found to have a dramatic effect on downtime of the mill. Prior to installation and employment of the inventive method of removing contaminants, the plant typically experienced about 10 hours of downtime per month due to stickies. After employment of the claimed process, the plant has run for eight months *without*
15 *a stoppage due to stickies*. In preferred embodiments the present invention is thus directed to a method of removing stickies from secondary or recycle fiber.

In one preferred mode of practicing the invention there is provided a method of processing papermaking fibers with a multistage array of forward cleaners
20 including a plurality of centrifugal cleaners configured to generate accepts streams and rejects streams which concentrate hydrophobic contaminants including the steps of: (a) feeding a first aqueous feed stream including papermaking fibers to a first stage bank of centrifugal cleaners of the multistage array; (b) generating a first accepts aqueous stream and a first rejects aqueous stream in the first stage bank of
25 centrifugal cleaners, the first aqueous rejects stream being enriched in hydrophobic contaminants with respect to the first aqueous feed stream; (c) supplying the first rejects aqueous stream to a flotation stage; (d) treating the first rejects aqueous stream in the flotation stage to remove hydrophobic waste from the first aqueous rejects stream and produce an intermediate aqueous purified feed stream; (e) feeding the

aqueous purified intermediate feed stream to a second stage bank of centrifugal cleaners of the multistage array, the second centrifugal cleaner being configured to generate a second accepts aqueous stream; and (f) combining the first accepts aqueous stream with the second accepts aqueous stream to form a combined accepts stream. A further step involves thickening the combined accepts stream. Generally, the process is carried out at a consistency of less than about 1%; typically at from about 0.3% to about 0.9%, and preferably at from about 0.4% to about 0.7%. The multistage array of forward cleaners comprises at least 3 banks of centrifugal cleaners in one embodiment.

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Hydrophobic contaminants removed from the first aqueous rejects stream by the flotation stage may include an ink composition, such as a toner ink composition. Typically, the hydrophobic contaminants removed from the first aqueous rejects stream by the flotation stage includes stickies, and may include an ink composition and stickies. The process is also believed unexpectedly effective in removing stickies derived from pressure sensitive adhesives.

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In yet another aspect of the invention, there is provided a method of thin stock processing of secondary fiber to remove contaminants including the steps of: (a) screening a first aqueous stream including secondary papermaking fibers having a consistency of less than about 2.5% in a screening device with openings having a screening dimension of less than about 10 mils to generate a screened accepts aqueous stream; (b) feeding the screened accepts aqueous stream to a multistage array of cleaners configured to generate centrifugal cleaner accepts streams and centrifugal cleaner rejects stream which concentrate heavy hydrophobic contaminants, the rejects stream of at least one centrifugal cleaner being fed to another centrifugal cleaner; and (c) processing at least one centrifugal cleaner rejects stream of a centrifugal cleaner of the multistage array with a flotation stage to remove hydrophobic contaminants, the

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flotation stage thereby generating a flotation purified stream having a reduced hydrophobic contaminants content.

Unless otherwise indicated, terminology appearing herein is given its ordinary meaning; %, percent or the like refers, for example, to weight percent and “consistency” refers to weight percent fiber or solids as that term is used in papermaking. “Mils” refers to thousandths of an inch. The banks of centrifugal cleaners are typically hydrocyclone type cleaners.

10 Brief Description of Drawings

The invention is described in detail below with reference to numerous examples and the appended Figures wherein like numbers designate similar parts throughout and wherein:

15 **Figure 1** is a schematic of a conventional multistage forward centrifugal cleaner system wherein each bank of cleaners are designated by a conical element;

Figure 2 is a schematic diagram of a hybrid multistage forward cleaner/flotation apparatus and process of the present invention, wherein a flotation stage is provided to treat the second stage rejects stream;

Figure 3 is a schematic diagram of a hybrid multistage forward cleaner/flotation apparatus and process of the present invention wherein a flotation stage is provided to treat the first stage rejects stream;

25 **Figure 4** is a schematic diagram of a hybrid multistage forward cleaner/flotation apparatus and process of the present invention wherein a flotation stage is provided to treat the first stage rejects and third stage accepts;

Figure 5 is a schematic diagram illustrating an apparatus and process of the present invention wherein the hybrid system has dual forward cleaner banks in series and the rejects stream from both of the forward cleaner banks are provided to a flotation cell;

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Figure 6 is a side broken away view of a screen containing a slotted basket; and

Figure 7 is a plot of residual ink concentration versus location in the pulp cleaning system.

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Detailed Description

The invention is described in detail below for purposes of illustration and exemplification only. Such explanation of particular embodiments in no way limits the scope of the invention which is defined in the appended claims. Referring to **Figure 1**, there is shown a conventional forward cleaner system **10** of the type employed at a paper mill, for instance, as part of the cleaning process for processing secondary pulp into paper products. System **10** has five stages **12, 14, 16, 18** and **20** of banks of centrifugal cleaners interconnected in the manner shown. Such connections may include suitable piping, mixing tanks, holding vessels and the like (not shown) as may be convenient for operating the system. Pulp is fed at low consistency to the system at **22** to the first bank of cleaners **12** through inlet **24** and centrifugally treated in the first stage by a bank of hydrocyclones, for example, such that the accepts are fed forward at **26** to a thickener (or another cleaning device) at **28** whereas the rejects, concentrating the heavy, hydrophobic waste in the system are fed to second stage **14** at **28** for further treatment in a second stage made up of a second bank of centrifugal cleaners **14**. Diluent water is added to the rejects stream from the first stage as indicated at **30** in an amount suitable for the particular system or operating conditions. Stream **28** (first stage rejects) is thus fed to the second stage

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cleaners whereupon bank 14 of cleaners generates an accepts stream 32 and a rejects stream 34. Stream 32 is recycled to the feed 22 and makes up a portion of the material fed to the first stage bank of cleaners 12. The first bank of cleaners may be made up of 50 or more hydrocyclones depending on capacity and performance
 5 desired. Subsequent stages will each contain fewer cleaners than the previous stage depending upon the amount of rejects, until the final stage contains less than 10 cleaners.

Stream 34 is again enriched with respect to heavy components (with respect to
 10 stream 32) and is fed to the third stage 16 bank of cleaners for further processing. Diluent water may again be added at 36 if so desired to stream 34. Stage 16 generates another accepts stream 38 which is fed back to the second stage (stream 28) and another rejects stream 40 enriched in heavy hydrophobic components.

15 In like fashion, stream 40 is fed to the fourth stage 18 bank of cleaners at 42 where diluent water may again be added. The fourth stage generates another accepts stream 44 and another rejects stream 46. These streams have the rejects/accepts characteristics noted above.

20 Stream 46 is fed to yet another stage 20 of forward cleaners at 48 wherein stream 46 is divided into an accepts stream 50 and a rejects stream 52 as indicated on the diagram. Accepts stream 50 is recycled to the fourth stage as shown and rejects stream 52 is discarded or further processed if so desired. There is thus described a conventional forward cleaner system utilizing centrifugal cleaners in
 25 cascaded/refluxing fashion to concentrate the waste material and purify the pulp which is fed forward at a papermaking process to a thickening device or a cleaning device such as screens or a reverse cleaner.

In accordance with the present invention, a flotation stage is advantageously integrated into a multistage forward cleaner system to remove hydrophobic material and increase the cleaning efficiency. Flotation utilizes the phenomenon that the minerals which are present in the ground ore can partially be wetted, i.e., they are hydrophilic, while other parts of the minerals are hydrophobic. Hydrophobic particles have a clear affinity to air. Accordingly, finely distributed air is introduced into the solid-water-mixture so that the air will attach to the hydrophobic particles causing them to rise to the surface of the mixture or suspension. The hydrophobic particles, such as valuable minerals or the above-mentioned contaminants present in repulped stock suspensions, collect as froth at the surface of the suspension and are skimmed off with a suitable means such as a paddle or weir. The hydrophilic particles of the ore or stock suspension remain in the flotation vat. It is also possible to separate two or more useful minerals selectively by the flotation method, for example, in the separation of sulfidic lead/zinc ores. For controlling the surface properties of the minerals small amounts of additives of chemical agents are introduced such as, for example, foaming agents which will help to stabilize the air bubbles, so-called collecting agents which actually cause the hydrophobic effect and prepare the mineral particles for attachment to the air bubbles, and floating agents which temporarily impart hydrophilic properties to the hydrophobic minerals and later return the hydrophobic properties for selective flotation, as mentioned above. The latter are generally inorganic compounds, mostly salts, while the collectors are mostly synthetic organic compounds, and the foaming agents are oily or soapy chemicals such as fatty acid soap.

The apparatus of the present invention may utilize a variety of readily available components. The centrifugal cleaners, for example, are available from Ahlstrom (Noormarkku, Finland) or Celleco (Model 270 series) (Lawrenceville, Georgia, USA) and are arranged in banks as shown in **Figures 2-5**. The flotation stage, which may be multiple cells, are likewise readily available from Comer SpA

(Vicenza, Italy). Comer Cybercel® models FCB1, FCB3 and FCB4 are suitable as discussed further herein.

There is illustrated in **Figure 2** an apparatus **100** and method in accordance with the present invention. Apparatus **100** operates similarly to apparatus **10** in **Figure 1**. Like parts are given like numbers for purposes of brevity and only differences noted from the discussion above. The system **100** of **Figure 2** operates as described in connection with system **10** of **Figure 1** and is so numbered in the drawing except that system **100** has a flotation stage **75** for treating the rejects stream **34** of second stage cleaner **14**. Diluent water may be added at **36** as before, and hereafter, stream **34** is treated in the flotation stage to remove hydrophobic material. The accepts from the flotation stage, that is purified as shown by removing hydrophobic waste from stream **34**, is then fed in stream **34'** to third stage cleaner **16**. Instead of refluxing the accepts from the third stage back to the second stage, the accepts material is fed forward in a product stream **26'** for downstream processing. The hydrophobic rejects (**31'**) from flotation stage (**75**) are removed from system **100**.

In **Figure 3** there is illustrated another apparatus **200** and method of the present invention. Here again similar functioning parts are numbered as in **Figures 1** and **2**, the discussion of which is incorporated by reference here. Apparatus **200** of **Figure 3** differs from apparatus **10** of **Figure 1** in that a flotation stage **75** is added to treat the first stage rejects stream **28** to remove hydrophilic waste to produce an intermediate purified stream **28'** which is fed to the second stage bank of cleaners **14**. Bank **14** generates a purified accepts stream **32'** which is fed forward to the thickening or other device **28** along with stream **26**. The hydrophobic rejects (**21'**) from flotation stage (**75**) are removed from system **200**.

In **Figures 4** and **5** there are illustrated alternate embodiments of the present invention. Like components are numbered as in **Figures 1-3** above, the discussion of

which is incorporated by reference. In the apparatus 300 of **Figure 4**, there is provided a flotation cell 75 which treats rejects stream 28 from the first centrifugal cleaning stage along with accepts stream 38' from the third centrifugal cleaning stage. Stream 38' is combined with rejects stream 28 and fed to the flotation stage where hydrophobic material is removed and an intermediate purified stream 28' is produced. Stream 28' is fed to the second stage 14 of centrifugal cleaners. The accepts stream from stage 14 is fed forward as stream 32'' and combined with stream 26 in thickening device 28. The hydrophobic rejects (21') from flotation stage (75) are removed from system 300.

Apparatus 400 of **Figure 5** resembles apparatus 200 of **Figure 3** except that there is provided a preliminary stage 12' of centrifugal cleaners, the accepts stream 26'' of which is utilized as the feed to stage 12. Rejects stream 28'' of stage 12' is combined with rejects stream 28 of stage 12 and fed to flotation stage 75. Accepts stream 32' of the second stage cleaners is fed forward with accepts stream 26 of stage 12. The hydrophobic rejects (21') from flotation stage (75) are removed from system 400.

Examples

Pilot plant trials showed that flotation cells such as the Comer Cybercel ® can successfully deink secondary centrifugal cleaner rejects, with better results obtained if the consistency is kept close to 0.6%. Consistency refers to weight percent fiber or associated solids such as ash unless the context indicates otherwise. Results on 42% office waste (Grade A) and 100% office waste (Grade B) are shown in Table 1.

Table 1: Pilot Plant Results for Brightness Gain, Dirt + Ash Removal Efficiency on Grades A and B at Halsey and Results Used in Simulation Models

5	Grade:	<u>A</u>	<u>B</u>	<u>Model</u>
	Consistency:	0.69%	0.90%	0.62%
	Brightness Gain:	18.5%	5.3%	
	Dirt Removal:	77-89%	65-87%	80%
10	Ash removal:	63%	64%	64%

A simulation model was used to calculate the impact of a Comer Cybercel® flotation cell to deink forward cleaner rejects on solids loss, ash removal and on removal efficiency of mid-dirt (>150 microns) from a 1st washer to the deinked pulp
 15 (while running grade B at 336 tpd at the 1st washer):

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Table 2: Impact of Flotation Cell on Solids Loss, Ash Loss, and Mid-dirt Removal Efficiency

(according to the Simulation Model for 6 different configurations on Grade B)

Example	Solids loss	Ash loss	Mid-dirt Eff.
1 No Flotation cell	8.9 tpd	0.8 tpd	96.1%
2 Flotation cell on 2 nd stage Rejects	2.7 tpd	0.9 tpd	97.0%
3 Flotation cell on 1 st stage Rejects	6.7 tpd	1.9 tpd	97.4%
4 As 3 with 50% eff. in 1 st stage	6.7 tpd	1.9 tpd	97.7%
5 Flotation cell on 1 st stage Rejects + 3 rd stage accepts, 44% eff. in 1 st stage	8.9 tpd	1.9 tpd	97.7%
6 Flotation cell on two 1 st stages	11.8 tpd	2.8 tpd	98.5%

The following indicators were used to evaluate the performance of the pilot plant:

- feed consistency.
- brightness gain of handsheets from accepts compared to feed.
- Dirt removal efficiency of small dirt (<150 microns), mid-dirt (>150 microns) and large dirt (>200 microns).
- Ash removal efficiency.

The results in Table 3 below for examples 7-14 (duplicate runs) show that even at 0.90% feed consistency it was possible to obtain 5.3% points brightness gain,

73% mid-dirt removal efficiency and 64% ash removal on Grade B. Operating the flotation cell at 0.69% consistency on Grade A, it was possible to obtain 8.1% points brightness gain, 79% mid-dirt removal efficiency and 63% ash removal.

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Table 3: Comer Pilot Plant Results on 2nd stage Cleaner Rejects

Example	Anal.	Cons. %	Feed Ash %	Brightness Gain	Dirt + Ash Removal %				Comments
					Small	Mid	Large	Ash	
Grade B									
7	1	0.86		3.3	88	71	64		Accepts=90%>200 m.
	2		4.4%	5.8	87	74	65	59	
8	1	0.88		5.4	87	74	67		Accepts=99%>200 m.
	2		3.9%	4.6	86	69	57	52	
9	1	0.88		6.3	88	78	74		
	2		5.9%	5.0	87	73	66	68	
10	1	0.98		5.9	89	74	61		
			3.8%	5.7	86	69	63	77	
Average		0.90	4.5%	5.3	87	73	65	64	
Grade A									
11	1	0.53		7.3	-	-	-		Accepts=95%>200 m.
	2		15.9%	9.4	92	78	72		
12	1	0.83		4.2	88	70	60	70	Accepts=90%>200 m.
	2		17.8%	8.2	87	70	64		
13	1	0.70		8.6	89	88	92	53	Accepts=74%>200 m.
	2		16.5%	8.0	89	80	80		
14	1	-		8.7	91	85	87	67	
	2		23.8%	10.4	89	85	85		
Average		0.69	18.5%	8.1	89	79	77	63	

The effect of incorporating a flotation stage in accordance with the present invention into a multistage forward cleaner system was evaluated with a computer model with respect to the systems illustrated in **Figures 1-5**. Results are summarized in the tables below. DIP refers to deinked pulp and DRE refers to dirt removal efficiency.

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Table 4: System of Figure 1 - Conventional Multi-Stage Cleaner System

SUMMARY									
		Flow	Cons.	Ash	Ash	Dirt >150	Dirt >150	Dirt >150	
		gpm	%	STPD	STPD	ppm/1.2g	ppm/1.2g	m ² /day	
Washer	Thick Stock	540	10.37	2.53	8.5	720	720	3310	
	DWw	4272	0.03	7	0.5	1504	1504	158	
Gyro	Accept	4812	1.19	2.63	9.0	738	738	3468	
Gyro	Accept	4812	1.19	2.49	8.55	738	738	3468	
Dil.Water		4741	0.03	7.00	0.60	1504	1504	176	
Total In		9553		351.9	9.15			3644	
1 st Stage Cleaner	Accept	9492	0.60	343.0	8.34	596	596	2798	
Total out	Accept	9492		343.0	8.34	596	596	2798	
Diff.	In-out	60		8.9	0.8			846	
5 th Stage Cleaner	Rejects	60	2.46	8.9	0.80	6957	6957	847	
Total	Rejects	60		8.9	0.8			847	
	Cleaner to Press DRE:							30.0% DRE	
Dil.Water	Out	9334	0.03	16.8					
Press	Out	158.5	35.1	326.2	6.2	417	417	1863	
DIP	Press to DIP DRE:							93.3% DRE	
PROCESS	Washer - DIP							28	
								96.1% DRE	

Table 5: System of Figure 2 — Multi-Stage Cleaner System with Flotation Cell on 2nd Stage Rejects

SUMMARY									
		Flow	Cons.		Ash	Ash	Dirt >150	Dirt >150	
		gpm	%	STPD	%	STPD	ppm/1.2g	m ² /day	
Washer	Thick Stock	540	10.37	335.7	2.53	8.5	720	3310	
	DWW	4272	0.03	7.7	0.7	0.1	150.4	16	
Gyro	Accept	4812	1.19	343.4	2.49	8.5	708	3326	
Gyro	Accept	4812	1.19	343.4	2.49	8.55	708	3327	
	Dil.Water	5666	0.03	10.2	0.70	0.07	150	21	
Total In		10478		353.5		8.62		3348	
1 st Stage Cleaner	Accept	9492	0.57	327.0	2.25	7.34	461	2063	
	Accept	927	0.43	23.8	1.39	0.33	373	121	
Total out		10419	0.56	350.8		7.68	455	2185	
Comer	In-out	58		2.7		0.9		1164	
	Rejects	42	0.93	2.3	34.77	0.81	32762	1050	
5 th Stage Cleaner	Rejects	16	0.36	0.3	32.88	0.11	23680	113	
	Rejects	58		2.7		0.9		1163	
Cleaner to Press DRE:									
Dil.Water	Out	10261	0.03	18.5			30.0% DRE		
	Out	158.5	35.1	332.4	1.9	6.3	318	1449	
Press to DIP DRE:									
DIP							93.3% DRE		
							21.3		
PROCESS									
	Washer - DIP						97.0% DRE		

Table 6: System of Figure 3 – Multi-Stage Cleaner System with Flotation Cell on 1st Stage Rejects

SUMMARY		Flow	Cons.	Ash	Ash	Dirt >150	Dirt >150
		gpm	%	STPD	%	ppm/1.2g	m ² /day
Washer	Thick Stock	540	10.37	335.7	2.53	720	3310
	DWw	4272	0.03	7.7	0.7	150.4	16
	Accept	4812	1.19	343.4	2.49	708	3326
Gyro	Accept	4812	1.19	343.4	2.49	708	3327
	Dil.Water	7449	0.03	13.4	0.70	150	28
	Total In	12261		356.8			3355
1 st Stage Cleaner	Accept	9492	0.50	282.9	2.13	443	1715
	Accept	2679	0.42	67.1	1.12	191	175
	Accept	12171	0.48	350.1		394	1890
2 nd Stage Cleaner	Diff.	90		6.7		1.85	1465
	Rejects	74	1.45	6.4	25.91	15279	1337
	Rejects	16	0.28	0.3	69.31	34056	128
5 th Stage Cleaner	Total	90		6.7		1.85	1465
	Cleaner to Press DRE:					30.0% DRE	
	Out	12012	0.03	21.6			
Dil.Water Press	Out	158.5	35.1	328.5	1.9	276	1241
	Press to DIP DRE:					93.3% DRE	
	DIP					18.5	
PROCESS	Washer - DIP					97.4%	DRE

Table 7: System of Figure 4 – Multi-Stage Cleaner System with Flotation on 1st St. Rejects + 3rd St. Accepts

SUMMARY									
		Flow	Cons.	Ash	Ash	Dirt >150	Dirt >150	Dirt >150	
		gpm	%	STPD	%	ppm/1.2g	m ² /day		
Washer	Thick Stock	546	10.37		2.51	8.52	6921		
	DWw	4266	0.015	3.8	0.7	0.0	16		
Gyro	Accept	4812	1.19	343.4	2.49	8.55	6937		
Gyro Dil.Water	Accept	4812	1.19	343.4	2.49	8.55	6937		
		7543	0.015	6.8	0.70	0.05	28		
Total In		12355		350.1		8.60	6965		
1 st Stage Cleaner	Accept	10100	0.46	279.2	2.15	6.01	3118		
	Accept	2104	0.50	62.9	1.16	0.73	298		
2 nd Stage Cleaner	Accept	12204	0.47	342.2	1.97	6.74	3416		
Diff.		151		8.0		1.9	3549		
Comer	Rejects	143	0.91	7.8	23.75	1.85	31464		
	Rejects	8	0.41	0.2	7.68	0.02	202		
Total		151		8.0		1.9	3549		
Cleaner to Press DRE:									
Dil.Water Press	Out	12045	0.015	10.8				30.0% DRE	
	Out	158.5	35.1	331.3	1.9	6.3	511	2316	
DIP	Press to DIP DRE:							Double-dirt	
								93.3% DRE	
PROCESS	Washer - DIP							34	
								Double-dirt	
								97.7% DRE	

Note: Mid-dirt level at the Gyro was doubled from 738 to 1476 ppm in this simulation, which results in double-dirt figures at the press and in the DIP. (L-wide by 2 for comparison with simulations in Tables 4-6).

Table 8: System of Figure 5 – Multi-Stage Cleaner System with Flotation Cell on both 1st Stage Rejects.

SUMMARY		Flow	Cons.	Ash	Ash	Dirt >150	Dirt >150
		gpm	%	STPD	ppm/1.2g	m ² /day	
Washer	Thick Stock	546	10.37				
	DWW	4266	0.015	8.5	1489	6920	
Gyro	Accept	4812	1.19	0.0	300	16	
				8.5	1476	6935	
Gyro	Accept	4812	1.19	8.55	1476	6937	
	Dil.Water	7431	0.015	0.05	300	27	
Total In		12243		8.60		6964	
1 st Stage Cleaner 2	Accept	8417	0.44				
	Accept	3619	0.53	4.21	523	1596	
2 nd Stage Cleaner	Accept	12036	0.47	1.56	388	612	
		12036	0.55	5.77	477	2208	
Diff.		208		2.8		4756	
Comer	Rejects	192	0.99				
	Rejects	16	0.39	2.81	28167	4389	
Total		208		0.03	71490	367	
				2.8		4756	
Cleaner to Press DRE:							30.0% DRE
Dil.Water	Out	11856	0.015				
	Out	180.0	35.16	0.1	334	1497	
Press to DIP DRE:							93.3% DRE
DIP							
					22		
Washer - DIP							98.5% DRE
PROCESS							

Note: Mid-dirt level at the Gyro was doubled from 738 to 1476 ppm in this simulation, which results in double-dirt figures at the press and in the DIP. (Divide by 2 for comparison with simulations in Tables 4-6).

The process of the present invention is particularly useful in connection with thin stock processing of recycle fiber, wherein the aqueous stream has a consistency of less than about 1% during such processing. Thin stock processing is employed in connection with commercial recycling operations, following pulping, thick stock
5 cleaning and washing prior to thickening and bleaching, for example. In a preferred thin stock process in accordance with the invention, the thin stock is screened in a screening device with a screening dimension of less than about 10 mils to generate a screened accepts aqueous stream which, in turn, is fed to a hybrid sytem such as shown in **Figure 4**, for example. The screening dimension of the screening device is
10 the slot width of a slotted screen basket, or could be the hole diameter of an alternate screening device.

Slotted screening devices are preferred and are well known. There is shown in **Figure 6** such a slotted screening device **500** provided with a feed port **510**, a
15 screen **520** provided with a plurality of elongated slots such as slots **530**, a rejects outlet **540** as well as an accepts outlet **550**. A feed stream is fed at **510** while the rejects stream is withdrawn at **540** and the screened accepts aqueous stream **560** exits outlet **550**. Accepts stream **560** may then be fed forward to a first stage bank of centrifugal cleaners for further dilution and processing as described above.

20

Slotted screens having a slot width of 8 mils or less may be employed. In commercial processes, fine slotted screens of 6 mils are frequently employed.

A commercial operation utilizing thin stock processing as part of its secondary
25 fiber processing was operated with a hybrid system as shown and described in connection with **Figure 4** above. The multistage array of forward cleaners was fed with thin stock which had been screened with 6 mil slotted screens prior to being fed to the forward cleaners. The particular arrangement included in sequence fine slotted screens, gyrocleans followed by the forward cleaner/flotation cell system. The

flotation cell employed was a Comer-Cybercell™ device which is preferably operated without diffuser plates. The system was installed along with expansion of a disk thickener downstream of thin stock processing of the fiber. As a result of this project the cleaners started performing better (improved dirt removal efficiency) and the hybrid cleaner-flotation cell removed approximately 80% of the dirt, 63% of the stickies and 53% of the ash in the Comer feed with a brightness increase of 2.4% points. Process mid dirt removal efficiency increased 2.4% (from 96.9% to 98.3%) when running mixed office waste (“MOW”) recycle fiber at 540 ton per day (tpd) input rate. The paper machines have run without stickies problems for 8 months since the Comer cell came on line.

The new treatment protocol operated well on a furnish containing 100% mixed office waste (MOW) as shown in Table 9, which compares mid dirt removal efficiency (MDRE)>0.02-0.5 mm² before and after Comer flotation cell start-up:

Table 9: Mid Dirt Removal Efficiency Before and After Start-up of Hybrid Cleaner – Comer Flotation Cell on a Furnish Containing 100% Mixed Office Waste (MOW)

Time Period	Mid Dirt Removal Efficiency of Dirt > 0.02 – 0.5 mm ²					
	Process	Cleaner	Comer-Cleaner	Thickener	Disperger	Disperger – DIP
Before Hybrid	96.4%	45%	53% - clnr	21%	74%	70%
After Hybrid	97.7%	50%	79%	13%	78%	73%

The Effective Residual Ink Concentration (ERIC) also improved throughout the whole deinking system as can be seen in **Figure 7**. ERIC levels in the deinked pulp dropped from 76 ppm without the inventive thin stock cleaning method to 21 ppm with the hybrid fiber when running MOW fiber at 365 tpd.

The performance of the hybrid cleaner – flotation cell is summarized in Table 10. It shows 2.4% points brightness increase, 82% total dirt removal efficiency (TDRE) and 53% ash reduction across the combination. The quality of the 2nd stage cleaner accepts was even better than the first stage cleaner accepts.

5

**Table 10: Hybrid Cleaner – Flotation Cell Results Operating On
1st Stage Cleaner Rejects**

10

Unit Operation	Feed			Brightness Gain	Dirt Removal Efficiency			Ash Removal
	Cons	Ash	Br.*		Small	MDRE	TDRE	
Comer	0.65%	2.0%	70.9%	2.0 % pts	78.8%	64.3%	71.0%	50%
St.2 Cleaner	0.58%	1.0%	72.9%	0.4 % pts	47.2%	51.2%	49.7%	10%
	Accepts							
Comer-clnr	0.49%	0.9%	73.3%	2.4 % pts	85.3%	79.1%	82.0%	53%

*Br. Is brightness of feed and accepts, MDRE is mid dirt removal efficiency and TDRE is total dirt removal efficiency.

In the plant, the number of stickies in the deinked pulp are counted 3 times per shift by screening a 150 gram sample of deinked pulp on a flat screen with 0.006 inch slots. The count for MOW based fiber averaged 3.3 stickies per 150 grams before installation of the hybrid system and improved to ~ 1.3 stickies per 150 grams after implementation of the process.

The area of stickies retained on a Pulmac® screen with 4 mil slots was also measured for selected samples. The uncompressed stickies are then counted using a microscope equipped with a grid to estimate the size of the stickies. Two sets of samples were obtained at 4 locations in the overall pulp-cleaning process at a first date, prior to installation and operation of the hybrid cleaner system (Data Set A), at 12 locations at a second date, also prior to installation of the hybrid cleaner system (Data Set B) and again at 8 locations in the process at a third date while the hybrid system shown in **Figure 4** was operating (Data Set C). The average results of 20

gram stock samples for each location are shown in Table 11. The improvement in total stickies removal efficiency from 95.0% to 98.5% is attributed in part to the improved operation of the hybrid forward cleaning system over forward cleaners alone.

5

Table 11: Comparative Stickies Removal

(Small stickies = <0.28 mm²; Large stickies = 0.28 – 1.47 mm²; X-Large stickies = >1.47 mm²)

Process Location and Data Set	Pulmac Stickies (mm ² /100 grams)				Total Removal Efficiency
	Small	Large	X-Large	Total	
Data Set A					
High Density Cleaner	72	219	119	409	
1 st Washer - out	76.9	51.3	10	138	1 st washer -DIP = 85.3%
Disperger - in	49.1	0	0	49	
Deinked Pulp	20.3	0	0	20	HDCI-DIP = 95.0%
Data Set B					
1 st Washer - out	64.0	13.3	0	77	1 st washer -DIP = 91.0%
Fine Slotted Screens - out	50.8	3.1	0	54	
St.1 Cleaner - in	42.9	0.5	0	43	
St.1 Cleaner - out	36.9	2.8	0	40	
St.2 Cleaner - out	43.6	0	0	44	
Disperger - in	48.9	2.7	0	52	
Disperger - out	31.9	0	0	32	
Deinked Pulp	6.8	0	0	7	
Data Set C					
High Density Cleaner	102	168	37	306	
1 st Washer - out	54.7	10.9	0	66	1 st washer -DIP = 93.0%
Fine Slotted Screens - out	53.1	0	0	53	
Comer cell - Feed	48.8	0	0	49	Comer in-out = 62%
Comer Cell - Accepts	18.1	0.6	0	19	
Disperger - in	35.9	0	0	36	Disp. in-out = 34%
Disperger - out	21.6	0	0	22	
Deinked Pulp	4.6	0	0	5	HDCI-DIP = 98.5%

10

It can be seen from Table 11 that the Comer cell was particularly effective in removing small stickies, removing over 60 percent of the stickies in the feed to the flotation cell.

1971	1972	1973	1974	1975
1976	1977	1978	1979	1980
1981	1982	1983	1984	1985
1986	1987	1988	1989	1990
1991	1992	1993	1994	1995
1996	1997	1998	1999	2000
2001	2002	2003	2004	2005
2006	2007	2008	2009	2010
2011	2012	2013	2014	2015
2016	2017	2018	2019	2020
2021	2022	2023	2024	2025
2026	2027	2028	2029	2030
2031	2032	2033	2034	2035
2036	2037	2038	2039	2040
2041	2042	2043	2044	2045
2046	2047	2048	2049	2050
2051	2052	2053	2054	2055
2056	2057	2058	2059	2060
2061	2062	2063	2064	2065
2066	2067	2068	2069	2070
2071	2072	2073	2074	2075
2076	2077	2078	2079	2080
2081	2082	2083	2084	2085
2086	2087	2088	2089	2090
2091	2092	2093	2094	2095
2096	2097	2098	2099	2100
2101	2102	2103	2104	2105
2106	2107	2108	2109	2110
2111	2112	2113	2114	2115
2116	2117	2118	2119	2120
2121	2122	2123	2124	2125
2126	2127	2128	2129	2130
2131	2132	2133	2134	2135
2136	2137	2138	2139	2140
2141	2142	2143	2144	2145
2146	2147	2148	2149	2150
2151	2152	2153	2154	2155
2156	2157	2158	2159	2160
2161	2162	2163	2164	2165
2166	2167	2168	2169	2170
2171	2172	2173	2174	2175
2176	2177	2178	2179	2180
2181	2182	2183	2184	2185
2186	2187	2188	2189	2190
2191	2192	2193	2194	2195
2196	2197	2198	2199	2200
2201	2202	2203	2204	2205
2206	2207	2208	2209	2210
2211	2212	2213	2214	2215
2216	2217	2218	2219	2220
2221	2222	2223	2224	2225
2226	2227	2228	2229	2230
2231	2232	2233	2234	2235
2236	2237	2238	2239	2240
2241	2242	2243	2244	2245
2246	2247	2248	2249	2250
2251	2252	2253	2254	2255
2256	2257	2258	2259	2260
2261	2262	2263	2264	2265
2266	2267	2268	2269	2270
2271	2272	2273	2274	2275
2276	2277	2278	2279	2280
2281	2282	2283	2284	2285
2286	2287	2288	2289	2290
2291	2292	2293	2294	2295
2296	2297	2298	2299	2300
2301	2302	2303	2304	2305
2306	2307	2308	2309	2310
2311	2312	2313	2314	2315
2316	2317	2318	2319	2320
2321	2322	2323	2324	2325
2326	2327	2328	2329	2330
2331	2332	2333	2334	2335
2336	2337	2338	2339	2340
2341	2342	2343	2344	2345
2346	2347	2348	2349	2350
2351	2352	2353	2354	2355
2356	2357	2358	2359	2360
2361	2362	2363	2364	2365
2366	2367	2368	2369	2370
2371	2372	2373	2374	2375
2376	2377	2378	2379	